

11. **(Original)** An apparatus as claimed in claim 10, wherein said supply is operable such that the oxygen concentration of the oxygen-containing gas introduced into said fluidized bed reactor is controlled to be from 0.1 to 0.3 of the theoretical amount of oxygen required for combustion of the wastes.

¹³/₁₂. **(Original)** An apparatus as claimed in claim ¹⁷/₁₃, further comprising at least one of sand, alumina, limestone and dolomite as a fluidized medium of said fluidized bed reactor.

¹²/₁₃. **(Original)** An apparatus as claimed in claim 1, wherein the partial combusting in said fluidized bed reactor is achieved by primary and secondary combustions, and the gasifying in said combustor is achieved by a tertiary combustion.

14. **(Original)** An apparatus as claimed in claim 1, operable at a pressure of 10 to 40 atmospheres.

15. **(Original)** An apparatus as claimed in claim 1, operable at a pressure of 30 to 40 atmospheres.

16. **(Original)** An apparatus as claimed in claim 1, wherein said temperature sufficient to melt said ash content of said char is at least 1300°C, and wherein said cooler comprises a quencher for removing the molten slag from said combustor and quenching the synthesis gas and molten slag by introducing the synthesis gas and molten slag directly into a liquid bath in a quenching chamber of said quencher.

17. **(Original)** An apparatus as claimed in claim 16, wherein said combustor includes a gasifying chamber and quenching chamber, the gasifying the gaseous material and the char is conducted in said gasifying chamber, and the quenching is conducted in said quenching chamber.